

Systems Analysis: Solutions to the Problems

Last update: 6 Jan 2012

1.1 Model formation

- a) System boundary = country border
External relations: immigration
Internal relations: birth rate, death rate, outmigration
- b) System boundary = planet Earth
External relations: none
Internal relations: birth rate, death rate
- c) System boundary = planetary surface and upper atmosphere
External relations: input from the ocean, mineralization / respiration of the biosphere, burning of fossil fuels
Internal relations: photosynthesis, transfer into the ocean
(also see Fig. 5.12)
- d) System boundary = water surface and boundary to the (non-reactive) sediment
External relations: Pb content of the sedimenting particles
Internal relations: re-solution of Pb via pore water into the lake, transfer into the non-reactive (deep) sediment

1.2 Solar system

- a) Gravitational forces between the planets and the sun
- b) None
- c) Gravitational forces between the solar system and other fixed stars (external relation)

1.3 From chemical elements to nuclear physics

- 1. Collecting: searching for chemical elements and their distinction from molecules
- 2. Organizing: finding elements with related properties, such as noble gases, alkaline metals, alkaline earth metals, etc.
- 3. Understanding: Bohr model of atoms, electron shells
- 4. Generalizing: quantum mechanics, Pauli principle for electrons
- 5. Predicting: completing the periodic system, transuranic elements

2.1 Mass balance

- a) $\frac{dM}{dt} = (\text{input from factory}) - (\text{transfer into atmosphere}) - (\text{chemical decomposition in the lake}) - (\text{outflow})$
- b) $\frac{dM}{dt} = (\text{transfer into atmosphere}) - (\text{sorption and sedimentation}) - (\text{chemical decomposition}) - (\text{outflow})$

Note: the substance mass entering the lake due to the accident is described by the initial condition $M_o = M(t=0)$.

2.2 Determining the dimension of parameters

$$[k_1] = \text{ML}^{-3} \text{T}^{-1}; [k_2] = \text{L}^2 \text{T}^{-1}; [k_3] = \text{L T}^{-1}; [k_4] = \text{M}^{-1} \text{L}^3 \text{T}^{-1}$$

2.3 Phosphorus sedimentation

10 m yr^{-1} , the mean „sinking velocity“ of phosphorus

2.4 Bed of nails

Bernoulli numbers for $n = 8$:

$$\frac{1}{256}, \frac{8}{256}, \frac{28}{256}, \frac{56}{256}, \frac{70}{256}, \frac{56}{256}, \frac{28}{256}, \frac{8}{256}, \frac{1}{256}$$

$$\text{Probability for box } m = 0: \frac{70}{256} = 0.273$$

3.1 Dimensional Henry coefficient

$$[K_H] = \text{L}^2 \text{T}^{-2}, \text{ Units e.g. } (\text{atm L mol}^{-1}) \text{ or } (\text{bar m}^3 \text{kg}^{-1})$$

$$K_{a/w} = \frac{K_H}{RT} \quad (R : \text{gas constant}, T : \text{absolute temperature})$$

3.2 Henry coefficient of methyl bromide

$$K_H = (6.5 \pm 0.5) \text{ atm L mol}^{-1}$$

$$K_{a/w} = \frac{(6.5 \pm 0.5)}{24.0} = 0.27 \pm 0.02 \quad (\text{with } R = 0.082 \text{ L atm mol}^{-1} \text{ K}^{-1}, T = 293 \text{ K})$$

3.3 Methyl bromide as ozone killer

Methyl bromide mass = 67.5 mol = 6.4 kg

3.4 Nonlinear sorption isotherm

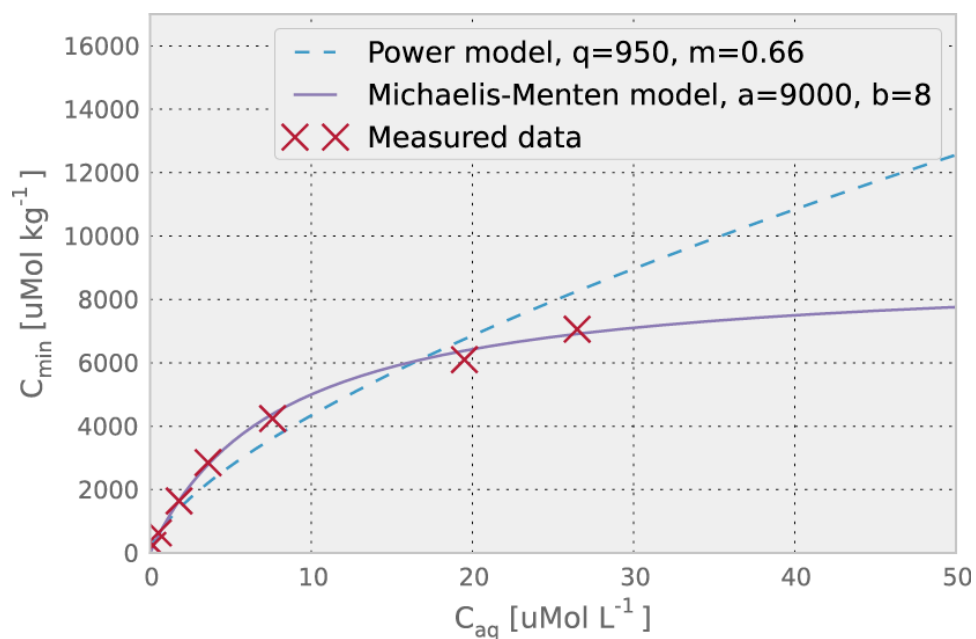
The usual expression for sorption equilibria has the form

$C_{min} = q (C_{aq})^m$. In double logarithmic form, this corresponds to a linear regression: $\ln(C_{min}) = m \cdot \ln(C_{aq}) + \ln q$.

The model is not entirely satisfactory. For higher concentrations, it systematically overestimates C_{min} (see figure). As alternative, we use the following model (Michaelis-Menten model):

$$C_{min} = a \cdot \frac{C_{aq}}{b + C_{aq}}$$

Here, the parameter a represents the saturation concentration and b the value of C_{aq} at which half of the (sorption) saturation is reached. This second model shows a much better fit to the measured data.

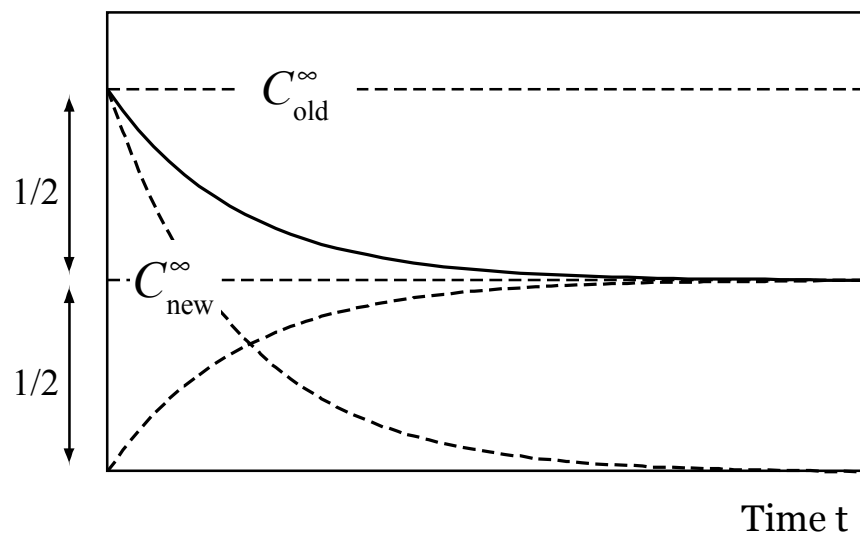


3.5 Economic theory: supply and demand

- a) Intercept point of the curves
- b) Price rises
- c) More machines sold, price sinks

4.1 Adjustment behavior

(as in Fig. 4.3)



4.2 Radioactive decay

a)
$$N_{\text{Rn}}(t) = N_{\text{Rn}}^{\infty} + (N_{\text{Ra}}^{\circ} - N_{\text{Rn}}^{\infty})e^{-\lambda_{\text{Rn}} t}$$

with $\lambda_{\text{Ra}} = 1.187 \times 10^{-6} \text{ d}^{-1}$, $\lambda_{\text{Rn}} = 0.1824 \text{ d}^{-1}$

$N_{\text{Rn}}^{\circ} = 5 \times 10^4 \text{ atoms/liter}$

$$N_{\text{Rn}}^{\infty} = \frac{\lambda_{\text{Ra}}}{\lambda_{\text{Rn}}} N_{\text{Ra}} = 650 \text{ atoms/liter}$$

b) $A_i = \lambda_i N_i$, $i = \text{Ra}, \text{Rn}$

$$A_{\text{Rn}}(t) = A_{\text{Rn}}^{\infty} + (A_{\text{Rn}}^{\circ} - A_{\text{Rn}}^{\infty})e^{-\lambda_{\text{Rn}} t}$$

with $A_{\text{Rn}}^{\infty} = A_{\text{Ra}} = 119 \text{ decays/liter/d}$

$A_{\text{Rn}}^{\circ} = 9.12 \times 10^3 \text{ decays/liter/d}$

4.3 Cars in a parking lot

- a) 425 parking spots
- b) 100 minutes
- c) 3.2 hours

4.4 Phosphorus in a lake with sedimentation

$C^\infty(10 \text{ t/yr}) = 40 \text{ mg m}^{-3}$ (i.e. the current state of the lake corresponds to the steady state of the current input)

$$C^\infty(6 \text{ t/yr}) = 24 \text{ mg m}^{-3}$$

$$\tau_{5\%} = 2.4 \text{ yr}$$

4.5 Exponential immigration

1975: Immigration $0.25 \times 10^6 \text{ yr}^{-1}$

2000: Immigration $1.19 \times 10^6 \text{ yr}^{-1}$

Population 35.1×10^6

4.6 Lake water temperature

a) $\frac{d\Theta}{dt} = (k_\Theta + k_w)(\Theta_{eq} - \Theta) = k(\Theta_{eq} - \Theta)$ with $k = (k_\Theta + k_w)$

b) Annual variation corresponds to $\omega = 0.017 \text{ d}^{-1}$

Lake A: $k_A = 0.03 \text{ d}^{-1} + 0.02 \text{ d}^{-1} = 0.05 \text{ d}^{-1}$

$$\eta_A = \arctan\left(\frac{0.017 \text{ d}^{-1}}{0.05 \text{ d}^{-1}}\right) = 18.8^\circ \quad ; \quad \Delta T_A \approx 19 \text{ days}$$

c) Lake B with identical thermal properties, without through-flow

Lake B: $k_A = 0.03 \text{ d}^{-1}$

$$\eta_A = \arctan\left(\frac{0.017 \text{ d}^{-1}}{0.03 \text{ d}^{-1}}\right) = 29.5^\circ \quad ; \quad \Delta T_A \approx 30 \text{ days}$$

d) $\frac{\Theta_{amp,A}}{\Theta_{amp}} = \frac{k_A}{\sqrt{k_A^2 + \omega^2}} = 0.947$; $\frac{\Theta_{amp,B}}{\Theta_{amp}} = \frac{k_B}{\sqrt{k_B^2 + \omega^2}} = 0.870$

$$\frac{\Theta_{amp,A}}{\Theta_{amp,B}} = 1.088$$

Lake A is better coupled to the annual temperature forcing and thus has slightly larger temperature amplitudes.

4.7 Dye in a well

$$\text{a) } \frac{dC}{dt} = -(k_r + k_w)C, \quad k_w = 0.06 \text{ h}^{-1}$$

$$C_0 = 5 \times 10^{-4} \text{ g/L}$$

$$\text{b) } t_{crit} = 24.5 \text{ h}$$

$$\text{c) } \frac{dC}{dt} = -k_r C, \quad t_{crit} = 39 \text{ h}$$

4.8 Degradation process in a sewage plant

$$\text{a) } \frac{dC}{dt} = k_w C_{in} - k_w C - R, \quad k_w = \frac{1}{\tau_w} = 0.5 \text{ d}^{-1}$$

$$\text{b) } \text{Since measurements show that } C^\infty = \frac{1}{20} C_{in}, \text{ it follows that } R = 19 k_w C^\infty$$

$$\text{c) } k_r = 19 k_w = 9.5 \text{ d}^{-1}$$

$$\text{d) } \tau_{5\%} = \frac{3}{k_r + k_w} = 0.15 \text{ d} = 3.6 \text{ h}$$

$$\text{e) } \tau_{5\%} = 0.15 \text{ d } (\tau_{5\%} \text{ does not change, since the system is linear!})$$

4.9 Copper accumulation on farm land

$$\text{a) } \frac{dm}{dt} = j - km \quad m: \text{Cu per m}^2$$

$$j: \text{Input per m}^2 \text{ and year}$$

$$k = 0.006 \text{ yr}^{-1}$$

$$\text{b) } m^\infty = 7000 \text{ mg m}^{-2}$$

$$\text{c) } \tau_{5\%} = 500 \text{ yr}$$

- d) $k = 0.007 \text{ yr}^{-1}$
- e) No, because input growth rate $\beta = 0.01$ is not $\ll k$

4.10 Tritium in a lake

The relevant parameters have the following values:

Decay constant of tritium: $k_\lambda = 0.058 \text{ yr}^{-1}$

$k_w = 0.1 \text{ yr}^{-1}$

$C_{in} \equiv C_{in}^\circ = 1 \text{ Bq/L}$ (Bq = Becquerel)

$C_{lake} = C^\circ = 0.44 \text{ Bq/L}$

- a) $\frac{dC}{dt} = k_w C_{in} - (k_w + k_\lambda) C = k_w C_{in} - k_t C, \quad k_t = k_w + k_\lambda$
- b) Since $\frac{C^\circ}{C_{in}} = 0.44$, $\frac{k_w}{k_w + k_\lambda} = 0.63$, there must be an additional elimination process.

Assumption: This elimination is first order with

$$k_r = k_w \frac{C_{in}}{C^\circ} - (k_w + k_\lambda) = 0.069 \text{ yr}^{-1}, \text{ i.e. } k_t = k_w + k_\lambda + k_r = 0.227 \text{ yr}^{-1}$$

- c) $C_{in}(t) = C_{in}^\circ e^{\beta t}$ with $\beta = 0.02 \text{ yr}^{-1}$
 $C(t = 10\text{yr}) = 0.50 \text{ Bq/L}, \quad C^\infty(t = 10\text{yr}) = 0.54 \text{ Bq/L}$

→ Perturbation by increasing input is nearly adiabatic.

- d) Like c), but with $\beta = \frac{1}{1 \text{ yr}} \ln(1.2) = 0.182 \text{ yr}^{-1}$
 $C(t = 10\text{yr}) = 1.53 \text{ Bq/L}, \quad C^\infty(t = 10\text{yr}) = 2.72 \text{ Bq/L}$

→ strongly non-adiabatic disturbance

5.1 Reactor with two substances

For parameters from Examples 5.2 and 5.3, in particular $k_w = 0.04 \text{ h}^{-1}$, t in $[\text{h}^{-1}]$:

$$C_1(t) [\text{mol m}^{-3}] = 0.091 - 0.0196 e^{-0.04t} - 0.0714 e^{-0.55t}$$

$$C_2(t) [\text{mol m}^{-3}] = 0.909 - 0.9804 e^{-0.04t} + 0.0714 e^{-0.55t}$$

5.2 Chain of lakes

$$\begin{aligned} \text{a) } \frac{dM_1}{dt} &= J_1 - \frac{Q_{1,2}}{V_1} M_1 - k_\lambda M_1 \\ \frac{dM_2}{dt} &= J_2 + \frac{Q_{1,2}}{V_1} M_1 - \frac{Q_2}{V_2} M_2 - k_\lambda M_2 \end{aligned}$$

This results in an identical coefficient matrix as in Eq. (5.34).

$$\text{b) } \frac{dM_{\text{tot}}}{dt} = J_1 + J_2 - k_\lambda M_{\text{tot}} - Q_2 C_2$$

The additional variable C_2 would be proportional to M_{tot} and could be replaced provided that (1) $J_2 = 0$; and (2) the system is at (quasi) steady state. Then the following holds:

$$C_2 = \frac{M_{\text{tot}}}{V_2 \left[1 + \frac{V_1}{Q_{1,2}} \left(\frac{Q_2}{V_2} + k_\lambda \right) \right]}$$

$$\text{c) } \text{Only the weighted sum of the concentration, } \bar{C} = \frac{C_1 V_1 + C_2 V_2}{V_1 + V_2} \text{ satisfies conservation of mass.}$$

5.3 Radioactive decay chain with three isotopes

$$\frac{dA_X}{dt} = -\lambda_X A_X \quad \lambda_X = 0.182 \text{ d}^{-1} = 7.6 \times 10^{-3} \text{ h}^{-1}$$

$$\frac{dA_Y}{dt} = \lambda_X (A_X - A_Y) \quad \lambda_Y = 1.55 \text{ h}^{-1}$$

$$\frac{dA_Z}{dt} = \lambda_Y (A_Y - A_Z) \quad \lambda_Z = 2.10 \text{ h}^{-1}$$

Since

$\lambda_Y, \lambda_Z \gg \lambda_X$, for times t with $t\lambda_Y \gg 1$ or $t\lambda_Z \gg 1$, the following approximation holds:
 $A_Y(t) : A_Z(t) : A_X(t) = A_X(0) e^{-\lambda_X t}$

5.4 Tritium in a sewage treatment plant

a)
$$\frac{dA_1}{dt} = -(k_{F1} + k_w + k_\lambda) A_1 + k_{F1} A_2$$

$$\frac{dA_2}{dt} = k_{F2} A_1 - k_{F2} A_2$$

$$k_\lambda = \frac{\ln 2}{\tau_{1/2}} = 1.58 \times 10^{-4} \text{ d}^{-1}, \quad k_w = \frac{Q}{V_1} = 1 \text{ d}^{-1}$$

$$k_{F1} = \frac{Q_F}{V_1} = 6 \times 10^{-3} \text{ d}^{-1}, \quad k_{F2} = \frac{Q_F}{V_2} = 0.02 \text{ d}^{-1}$$

b) Since k_λ is much smaller than other specific rates, decay plays no role

c) $\lambda_1 : -k_w, \quad \lambda_2 : -k_{F2}$

d) $A_1(t) = \text{const.} \exp(-k_{F2}t)$

5.5 Stratified lake with sedimentation

a) In V_1 : $\tau_w = 100 \text{ d}$; $\tau_{\text{ex},1} = 20 \text{ d}$; $\tau_{\text{tot}} = 16.7 \text{ d}$

In V_2 : $\tau_{\text{ex},2} = 40 \text{ d}$

b) through d)

	b) conservative	c) radioactive	d) conservative + sedimentating
Steady-state conc'ns:			
$C_1^\infty [\text{mg m}^{-3}]$	100	29	46
C_2^∞	100	21	54
Eigenvalues			
$\lambda_1 [\text{d}^{-1}]$	-0.00305	-0.0131	-0.0063
$\lambda_2 [\text{d}^{-1}]$	-0.0819	-0.0919	-0.104
$\tau_{50\%} : \frac{3}{ \lambda_1 } [\text{d}]$	980	230	480

e) Note that the smaller sedimentation rate in the deep water leads to a slightly increased concentration in the volume V_2 (case d).

5.6 Conservative substance in a chain of lakes

a) $C_1(t) = C_1^\circ e^{-k_{w1}t}$
 $C_2(t) = C_1^\circ \frac{k_{w2}}{k_{w1} - k_{w2}} (e^{-k_{w2}t} - e^{-k_{w1}t})$
 with $k_{w1} = \frac{Q_o}{V_1} = 1 \text{ d}^{-1}$, $k_{w2} = \frac{Q_o}{V_2} = 0.05 \text{ d}^{-1}$, $C_1^\circ = \frac{M}{V_1} = 2 \text{ gm}^{-3}$
 Adjustment times: $t_1 = 5.3 \text{ d}$, $t_2 = 46 \text{ d}$

b) $C_2^{\max} = 0.085 \text{ gm}^{-3}$, reached at time $t_{\max} = 3.2 \text{ d}$

c) $\alpha : k_{w2} = 0.05 \text{ d}^{-1}$

d) Eigenvalues of the system with pumping:

$$\lambda_1 = -5.2 \text{ d}^{-1}$$

$$\lambda_2 = -0.048 \text{ d}^{-1}$$

As a result of the high pumping power Q_p the system $(V_1 + V_2)$ can approximately be described as completely mixed, with the outflow rate

$$\frac{Q_o}{V_1 + V_2} = k_{\text{tot}} = 0.0476 \text{ d}^{-1} \sim -\lambda_2$$

and initial concentration $C_{\text{tot}}^\circ = \frac{M}{V_1 + V_2} = 0.095 \text{ gm}^{-3} = 95 \text{ mg m}^{-3}$

The critical concentration

$$C_{\text{krit}} = 10 \text{ } \mu\text{g/L} = 10 \text{ mg m}^{-3} \text{ is underrun after the time } t_{\text{krit}} = 47 \text{ d}.$$

e) See d).

5.7 Temperature control by a thermostat

a) $\frac{dy}{dt} = -L + k_1 x$; $\frac{dx}{dt} = k_2 (y_o - y)$

Purely imaginary eigenvalues $\lambda_i = \pm i(k_1 k_2)^{1/2}$

steady state at $y^\infty = y_o$, $x^\infty = L/k_1$ is not reached (undamped oscillations)

b) If equations are altered such that x cannot drop below 0, the system becomes nonlinear.

c) k_1 and k_2 should be large.

- d) The modification introduced in b) would dampen the oscillations. Alternatively, the 'valve equation' could be modified such that at large valve positions x the opening process is slowed down.

$$\frac{dx}{dt} = k_2(y_o - y) - k_\epsilon x$$

6.1 Mountain lake with time-dependent elimination rate

- a) System is linear
- b) No
- c) $j_{in}(t)$ und $k(t)$ are external relations
- d) Integration piece-wise for periods with $k = \text{const.}$, whereby the terminal value becomes the initial value of the next period.

6.2 Fish in a pond

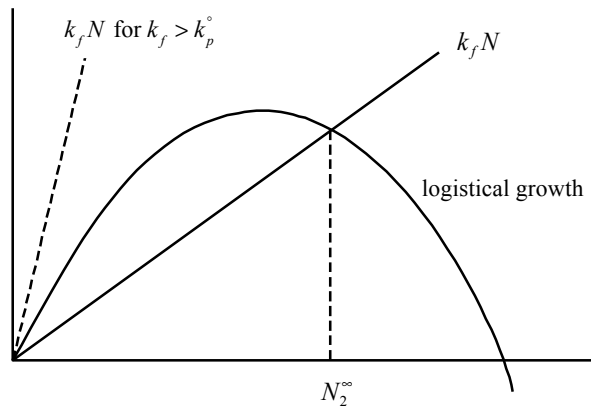
Note: The problem refers to Example 6.2 in Section 6.1.3.

a)
$$\frac{dN}{dt} = k_p^\circ N \left(1 - \frac{N}{N_{\max}} \right) - k_f N$$

Fixed point: $N_1^\infty = 0$, $N_2^\infty = \frac{k_p^\circ - k_f}{k_p^\circ} N_{\max}$

If $k_p^\circ > k_f$ (see question d), N_1^∞ is unstable, N_2^∞ stable.

b)



c) $k_f = \frac{1}{2} k_p^\circ$. Then, the yield is $Y = k_f N_2^\infty = k_f \frac{N_{\max}}{2}$

d) $k_p^\circ > k_f$

6.3 Jacobian matrix of the Lotka-Volterra model

$$B(X, Y) = \begin{pmatrix} (k_1 - k_3 Y) & -k_3 X \\ k_3 Y & (-k_2 + k_3 X) \end{pmatrix}$$

$$B(X_1^\infty = 0, Y_1^\infty = 0) = \begin{pmatrix} k_1 & 0 \\ 0 & -k_2 \end{pmatrix}$$

The fixed point is a saddle point (Fig. 6.11c) with stability along the Y axis, instability along the X axis.

$$B\left(X_2^\infty = \frac{k_2}{k_3}, Y_2^\infty = \frac{k_1}{k_3}\right) = \begin{pmatrix} 0 & -k_2 \\ k_1 & 0 \end{pmatrix}$$

Eigenvalues $\lambda_j = \pm i(k_1 k_2)^{1/2} \rightarrow$ center (Fig. 6.11f)

Note: It can be shown that the model exhibits an undamped oscillation (see Fig. 6.19c).

6.4 Predator-prey model with self-interaction

$$\text{Jacobian matrix } B(X, Y) = \begin{pmatrix} (k_1 - k_3 Y - 2k_4 X) & -k_3 X \\ k_3 Y & (-k_2 + k_3 X) \end{pmatrix}$$

At the fixed point $X_2^\infty = \frac{k_2}{k_3}$, $Y_2^\infty = \frac{k_1}{k_3} - \frac{\varepsilon}{k_3}$ with $\varepsilon = \frac{k_2 k_4}{k_3}$:

$$B(X_2^\infty, Y_2^\infty) = \begin{pmatrix} -\varepsilon & -k_2 \\ (k_1 - \varepsilon) & 0 \end{pmatrix}$$

$$\text{Eigenvalues } \lambda_j = \frac{1}{2} \left[-\varepsilon \pm \left\{ \varepsilon^2 + 4\varepsilon k_2 - 4k_1 k_2 \right\}^{1/2} \right]$$

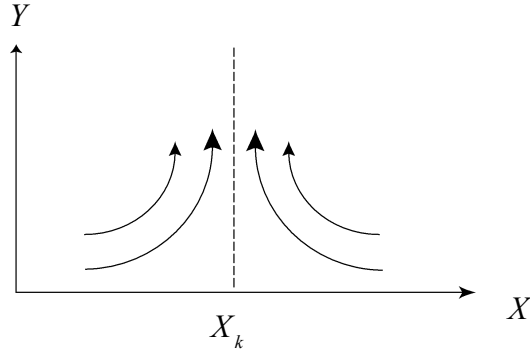
If k_4 is so small that $k_1 k_2 > \frac{\varepsilon^2}{4} + \varepsilon k_2$, then the eigenvalues are conjugate-complex with negative real part (case d in Fig. 6.11, also see Fig. 5.11a).

6.5 Semi-trivial fixed point of the Holling-Tanner model

$$\text{Jacobian matrix } \mathbf{B}(X_k, Y=0) = \begin{pmatrix} -r & -w \frac{X_k}{X_k + K_B} \\ 0 & s \end{pmatrix}$$

$$\text{Eigenvalues: } \lambda_1 = -r, \quad \lambda_2 = s \quad (r, s > 0)$$

→ Case c) in Fig. 6.11 (saddle point)



6.6 Nonlinear biomass growth in a pond

Note that f_w has the dimension $[(\text{concentration})^{-2} \text{T}^{-1}]$.

The solution to this problem becomes clearer if we replace the variable pair (N, B) by $(M = N + B, N)$.

- c) If condition (I) of answer d) is met, then the system has three fixed points:

$$(A) \quad M_A^\infty = \frac{J_N}{Q}, \quad N_A^\infty = \frac{J_N}{Q} \quad (i.e. \ B_A^\infty = 0)$$

$$(B) \quad M_B^\infty = M_A^\infty = \frac{J_N}{Q}; \quad N_B^\infty = \frac{1}{2}(N_0 - N_{crit})$$

$$(C) \quad M_C^\infty = M_A^\infty = \frac{J_N}{Q}; \quad N_C^\infty = \frac{1}{2}(N_0 + N_{crit})$$

$$\text{with } N_{crit} = \left(N_0^2 - 4 \frac{k_a + k_q}{f_w} \right)^{1/2}, \quad k_q = \frac{Q}{V}$$

stability → see d)

d) **Condition I:** biomass B can only be created if

$$N_0 \geq 2 \left(\frac{k_a + k_q}{k_w} \right)^{1/2}, \quad \text{i.e. } N_{crit} \text{ is real}$$

Fixed point (A) is stable for $\frac{J_N}{Q} < N_B^\infty$ and $\frac{J_N}{Q} > N_C^\infty$

Fixed point (C) is stable for $N_B^\infty \leq \frac{J_N}{Q} \leq N_C^\infty$

Fixed point (B) is unstable.

6.7 Lotka-Volterra with two prey animals

$$\begin{aligned} \text{a) } \frac{dX_1}{dt} &= k_1 X_1 - k_4 X_1 Y \\ \frac{dX_2}{dt} &= k_2 X_2 - k_5 X_2 Y \\ \frac{dY}{dt} &= k_4 X_1 Y + k_5 X_2 Y - k_3 Y \end{aligned}$$

b) 3 fixed points

(I) Trivial fixed point $X_1 = X_2 = Y = 0$

stable with respect to Y , unstable with respect to X_1 and X_2

$$\text{(II) } X_1^\infty = \frac{k_3}{k_4}, \quad X_2^\infty = 0, \quad Y^\infty = \frac{k_1}{k_4}$$

Center if $\frac{k_1}{k_4} > \frac{k_2}{k_5}$, otherwise unstable

$$\text{(III) } X_1^\infty = 0, \quad X_2^\infty = \frac{k_3}{k_5}, \quad Y^\infty = \frac{k_2}{k_5}$$

Center if $\frac{k_1}{k_4} < \frac{k_2}{k_5}$, otherwise unstable

c) Species with a higher growth/predation coefficient

$\left(\frac{k_1}{k_4} \text{ for } X_1, \frac{k_2}{k_5} \text{ for } X_2 \right)$ survives. In our example, X_2 survives

although X_1 has a higher growth rate ($k_1 > k_2$).

Predation pressure on X_2 is smaller than on X_1 ($k_5 < k_4$).

6.8

Lotka-Volterra with prey niche

$$\begin{aligned} \text{a) } \frac{dX_1}{dt} &= (k_1 - k_4)X_1 + k_5X_2 - k_3X_1Y \\ \frac{dX_2}{dt} &= (k_1 - k_5)X_2 + k_4X_1 \\ \frac{dY}{dt} &= k_3X_1Y - k_2Y \end{aligned}$$

b) For $k_1 < k_5$ the following non-trivial fixed point exists:

$$\begin{aligned} X_1^\infty &= \frac{k_2}{k_3}, & X_2^\infty &= \frac{k_2k_4}{k_3(k_5 - k_1)} \\ Y^\infty &= \frac{k_1(k_5 - k_1 + k_4)}{k_3(k_5 - k_1)} \end{aligned}$$

c) If $k_1 > k_5$, the prey in the niche (B_2) could increase unchecked, and then (by migrating out of the niche) help the predator achieve infinite growth. We can “fix” this behavior by replacing the linear prey growth by a logistical function:

$$i = 1, 2 \quad k_1X_i \rightarrow k_1^* \frac{X_i}{X_i + X_{krit}}$$

6.9

Competition for living space

$$\begin{aligned} \text{a) } \frac{dA}{dt} &= k_1A - k_2AB \equiv f_A(A, B) \\ \frac{dB}{dt} &= (k_3 - k_4B)B - k_5AB \equiv f_B(A, B) \end{aligned}$$

b) Fixed points:

$$\begin{aligned} (1) \quad A_1^\infty &= 0 \quad ; \quad B_1^\infty = 0 \\ (2) \quad A_2^\infty &= \frac{k_3}{k_5} - \frac{k_4k_1}{k_2k_5} = 2 \quad ; \quad B_2^\infty = \frac{k_1}{k_2} = 1 \\ (3) \quad A_3^\infty &= 0 \quad ; \quad B_3^\infty = \frac{k_3}{k_4} \end{aligned}$$

c) Stability of fixed point 2 (A and B non zero).

$$\text{Jacobian matrix } B(A, B) = \begin{pmatrix} 0 & \frac{1}{k_5}(k_2 k_3 - k_1 k_4) \\ -k_5 \frac{k_1}{k_2} & -\frac{k_1 k_4}{k_2} \end{pmatrix} = \begin{pmatrix} 0 & 2 \\ -4 & -4 \end{pmatrix}$$

Eigenvalues: $\lambda_{1,2} = -2 \pm 2i$ (damped oscillations)

7.1 Elimination of the inhomogeneous term

1-dimensional: With $\hat{\mathcal{V}}^{(n)} = \mathcal{V}^{(n)} + \frac{I}{a_0 - 1}$ it follows that $\hat{\mathcal{V}}^{(n+1)} = a_0 \hat{\mathcal{V}}^{(n)}$

q-th order: prove Eq. (7.17).

7.2 Consumer loan

$$(1.025)^{12} = 1.345 \quad \rightarrow \quad \text{annual interest } 34.5\%$$

7.3 Reactor with chloride

- a) 50 kg
- b) 14 weeks

7.4 Returnable bottles

- a) Use the method of the characteristic equation.
- b) Because the system is linear, we can choose a different approach for the first year and simply combine that with the original result, whereby the index n is moved by a month:

$$N^{(n)} = N_1^{(n)} + N_2^{(n)} \quad \text{with}$$

$$N_1^{(n)} = 5,300 \left[(\lambda_1)^n - (\lambda_2)^n \right]$$

$$N_2^{(n)} = 50,000 - 48,850(\lambda_1)^{n-1} - 1,150(\lambda_2)^{n-1}; \quad n \geq 1$$

$$\lambda_1 = 0.822, \quad \lambda_2 = -0.122$$

7.5 Fibonacci numbers

$$y^{(n)} = \frac{1}{\sqrt{5}} \left[(\lambda_1)^n - (\lambda_2)^n \right]$$

$$\text{with } \lambda_1 = \frac{1}{2}(1 + \sqrt{5}); \quad \lambda_2 = \frac{1}{2}(1 - \sqrt{5})$$

7.6 Gambling

a) $Y^{(0)} > 2X^{(0)}$

b) $Y^{(0)} = 2X^{(0)}$

7.7 Students in a study program

550

7.8 Fish in a pond

b) $N_1^{(i)} = 10,000 + 0.5 N_1^{(i-1)} + 2 N_2^{(i-1)}$

$$N_2^{(i)} = 0.1 N_1^{(i-1)}$$

c) Use $N_2^{(i-1)} = 0.1 N_1^{(i-2)}$

$$\rightarrow 10,000 - N_1^{(i)} + 0.5 N_1^{(i-1)} + 0.2 N_1^{(i-2)} = 0$$

d) $N_1^{(1)} = 10,000; \quad N_1^{(2)} = 15,000; \quad N_1^{(3)} = 19,500$

$$N_1^{(4)} = 22,750; \quad N_1^{(5)} = 25,275$$

e) $\hat{N}_1^{(i)} = N_1^{(i)} - 33,333.3$ makes the equation homogeneous.

Characteristic exponents:

$$\lambda_{1,2} = \frac{1}{2} (0.5 \pm \sqrt{1.05})$$

Initial values: note that $N_2^{(0)} = 0$ corresponds to $N_1^{(-1)} = 0$.

$$N_1^{(i)} = 33,333.3 - 31,305.3 (\lambda_1)^i - 2,028.0 (\lambda_2)^i$$

f) $N_1^{(\infty)} = 33,333.3$
 $N_2^{(\infty)} = 3,333.3$

8.1 Tetrachloroethylene in a pond

- a) 69 d
b) 34.5 d

8.2 Oxygen in the lake

This problem relates to Example 8.2 in Section 8.2.5.

Initially, C_A increases slightly (steady state concentration 12.8 mg/L) but as the deep water becomes anoxic, decreases to the slightly lower steady state value of 11.7 mg/L.

8.3 Geothermal heat flux at the bottom of a lake

- a) With $\frac{dT}{dx} = 0.175 \text{ km}^{-1}$ (x : Depth in the sediment, positive downwards)
we get $F_{th} = -0.10 \text{ Wm}^{-2}$ (Flux, positive upwards)

(Caution: the correct unit for γ_{th} is $\text{Wm}^{-1}\text{K}^{-1}$)

- b) $\frac{dT}{dz} = +4.8 \times 10^{-3} \text{ km}^{-1}$ (temperature increases with water depth z .)

8.4 Vertical turbulent diffusivity

- a) $K_z = 2.0 \text{ m}^2\text{d}^{-1} = 2.32 \times 10^{-5} \text{ m}^2\text{s}^{-1}$
b) $F_{Rn} = 3.0 \times 10^4 \text{ Bq m}^{-2}\text{d}^{-1}$

8.5 Péclet und Damköhler numbers

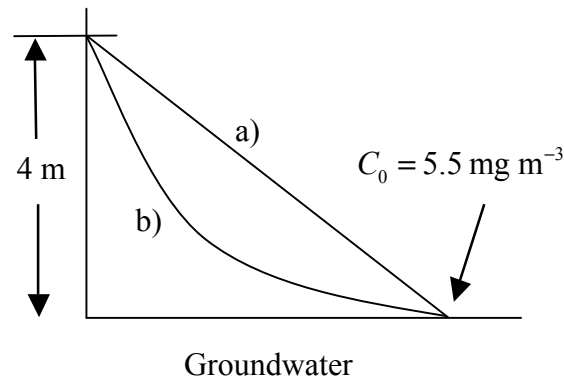
- a) $\frac{\tau_{diff}}{\tau_{ad}} = \frac{x_L^2 / 2D}{x_L / v} = \frac{1}{2} \frac{x_L v}{D} = \frac{1}{2} \text{ Pe}$

$$b) \quad \left(\frac{x_{diff}}{x_{ad}} \right)^2 = \frac{2D/k_r}{(v/k_r)^2} = 2 \frac{Dk_r}{v^2} = 2 \text{ Da}$$

(the factor 2 plays no role for this type of consideration!)

8.6 Volatile substance in the groundwater

a) + b)



$$c) \quad F = 1.4 \times 10^{-3} \text{ mg m}^{-3} \text{ d}^{-1}$$

$$d) \quad \tau_{diff} = 1143 \text{ d} = 3.1 \text{ yr}$$

e) $Pe = 57$, that is, transport flux is dominated by advection

$$\tau_{adv} = 40 \text{ d}$$

$$F_{adv} = 0.15 \cdot v C_0 = 0.083 \text{ mg m}^{-3} \text{ d}^{-1}$$

8.7 Transport and reaction in a lake's water column

a) Chemical A = Curve 4; B = 2; C = 3; D = 1

b) Vertical transport equation of chemical A and D. For chemical A, the first-order reaction rate $k_r = 0$. z is vertical coordinate, $z = 0$ at water surface.

$$\frac{\partial C}{\partial t} = -k_r C + D \frac{d^2 C}{dz^2} = 0$$

Solution for chemical A:

$$C(z) = C_0 + az. \text{ Since } \left. \frac{\partial C}{\partial z} \right|_{z=z_b} = 0 \text{ (no flux at sediment!)}, \text{ we get } a = 0.$$

For chemical D:

$$C(z) = p e^{\lambda z} + q e^{-\lambda z}, \quad \lambda = \left(\frac{k_r}{D} \right)^{1/2}$$

From the boundary conditions $C(z=0) = C_0$ and

$$\left. \frac{\partial C}{\partial z} \right|_{z=z_b} = 0, \text{ the coefficients } p \text{ and } q \text{ are:}$$

$$p = C_0 \frac{e^{-\lambda z_b}}{e^{\lambda z_b} + e^{-\lambda z_b}} \quad ; \quad q = C_0 \frac{e^{\lambda z_b}}{e^{\lambda z_b} + e^{-\lambda z_b}}$$

Inserting p and q yields:

$$C(z) = C_0 \frac{\cosh[\lambda(z - z_b)]}{\cosh[\lambda z]}$$

- c) For fast reaction ($k_r \rightarrow \infty$), the concentration in those layers in which reaction occurs drops sharply. Thus, at the sediment surface the curves for the reactive chemicals (B,C,D) are virtually zero. The concentration of chemical B drops linearly through the thermocline to virtually zero at the oxic/anoxic interface. Chemical C drops sharply from C_0 at the surface to virtually zero and remains small in the rest of the water column. D has the same profile as C, since nothing will be left for reaction in the deep anoxic layer.

8.8

Radium and tritium in the ocean deep water

	F_{deep}^{ad}	F_{deep}^{diff}	F_{sur}^{ad}	F_{sur}^{diff}	Decay	Sum
Radium	2.00	0.61	0	-1.60	-1.01	0
Tritium	0	0	-2.0	14.7	-12.7	0

Note: the numbers in the table are generalized transfer velocities in $[\text{m yr}^{-1}]$. If we multiply them by the corresponding boundary values (C_{BW} for radium, C_{OW} for tritium, in $[\text{Bq m}^{-3}]$), we get the fluxes in $[\text{Bq m}^{-2} \text{a}^{-1}]$.

8.9

Time-dependent diffusion/advection equation

Note: $\frac{\partial}{\partial t} C(x - v_x t) = -v_x C'$ with $C' = \frac{dC(\xi)}{d\xi}$

$$\frac{\partial}{\partial x} C(x - v_x t) = C'$$

8.10

Symmetrical diffusion at a boundary surface

$$C(x, t) = \frac{C_0}{2} \operatorname{erfc} \left(\frac{x}{2(D_x t)^{1/2}} \right), \text{ boundary at } x = 0$$

Note: $C(x = 0, t) = \frac{C_0}{2}$ (for all times $t > 0$)